



COMSOL
CONFERENCE
2015 BOSTON



A 1-D Model of the 4 Bed Molecular Sieve of the Carbon Dioxide Removal Assembly

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Component 1 (comp1) P_i $a = f(x)$ Transport (D1) (chcs) Mesh 1 Initial vapor pressure

Model Builder

- Global Definitions
 - Parameters
 - a= Glass
 - a= 13X_G544_old
 - a= Silica_Gel_B125
 - a= 5A_RK38
 - a= 5A_ASRT
 - a= Silica_Gel_Sorbead_WS
 - AL 6061 Thermal Cond (Cond)
 - AL 6061 Heat Capacity (HeatCap)
 - AL 6061 Density (Can0Density)
 - Vapor Pressure Low (VPL)
 - Vapor Pressure High (VPH)
 - Dew Point Low (DPL)
 - Dew Point High (DPH)
 - sorbent bed desorption pressure 10minAS (DesTotPressoft_10minAS)
 - Step for MassFracandFlux_S_Ads_influent (step)
 - Step for T_S_Ads_influent (step2)
 - Step for P_S_Ads_effluent (step3)
 - Interpolation 29 (DesTotPressoft_10minAS_baseline)
 - Materials
- Component 1 (comp1)
 - Definitions
 - Geometry 1
 - Materials
 - Transport (D1) (chcs)
 - Transport (D2) (tcs)
 - Transport (S1) (tcs2)
 - Transport (S2) (tcs3)
 - Heat Transfer in Can (D1) (ht2)
 - Heat Transfer in Can (D2) (ht)
 - Heat Transfer in Can (S1) (ht3)
 - Heat Transfer in Can (S2) (ht4)
 - Heat Transfer in Sorbent (D1) (ht5)
 - Heat Transfer in Sorbent (D2) (ht7)
 - Heat Transfer in Sorbent (S1) (ht8)
 - Heat Transfer in Sorbent (S2) (ht9)
 - Heat Transfer in Fluid (D1) (ht6)
 - Heat Transfer in Fluids (D2) (ht10)
 - Heat Transfer in Fluids (S1) (ht11)
 - Heat Transfer in Fluids (S2) (ht12)
 - Darcy's Law (D1) (dl)
 - Darcy's Law (D2) (dl2)
 - Darcy's Law (S1) (dl3)
 - Darcy's Law (S2) (dl4)
 - Loading (D1) (g)
 - Loading (D2) (g2)
 - Loading (S1) (g3)
 - Loading (S2) (g4)
 - Heater Switch (S1) (ge)
 - Heater Switch (S2) (ge2)
 - Insulation (D1) (ht15)
 - Insulation (D2) (ht16)
 - Insulation (S1) (ht13)
 - Insulation (S2) (ht14)
 - Multiphysics
 - Mesh 1
 - Initial
 - 2nd and further HalfCycles

Settings

Study

- Compute Update Solution

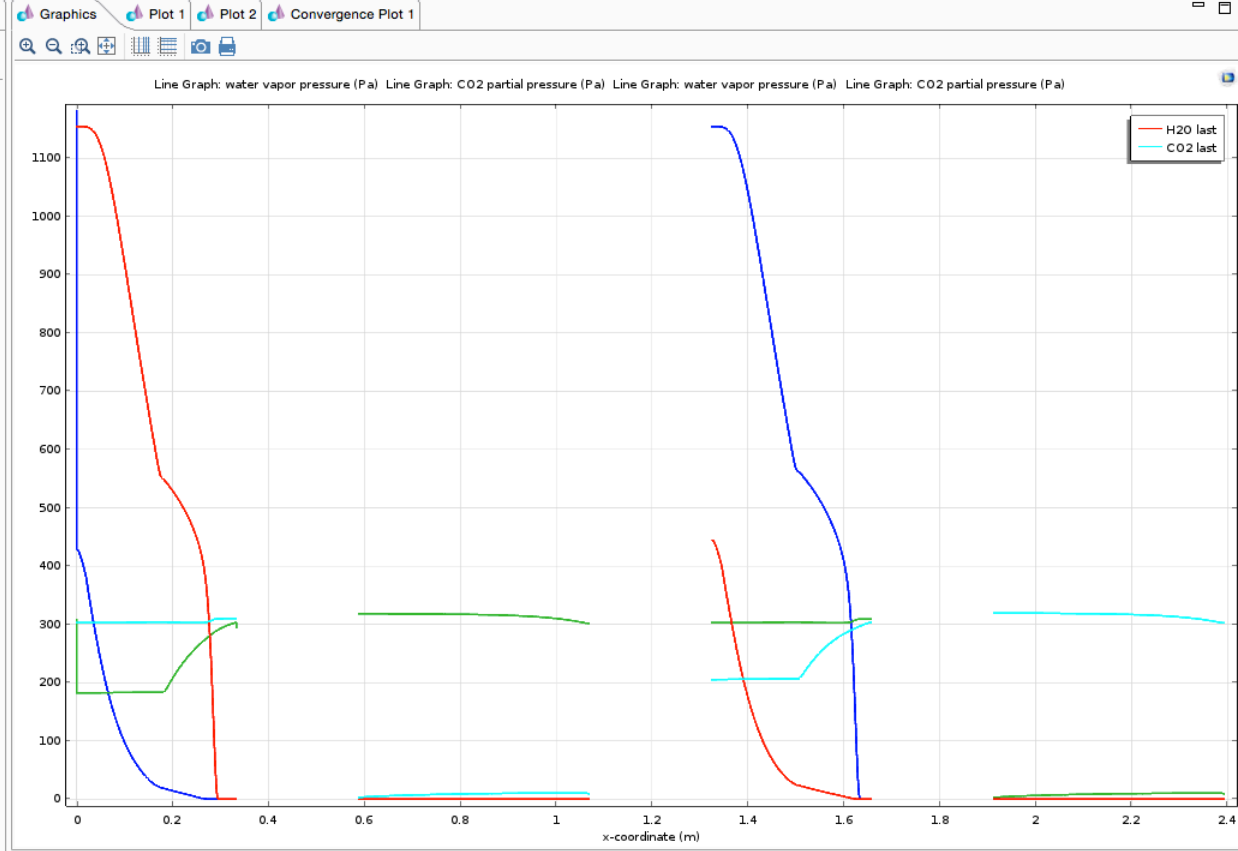
Label: Initial

Study Settings

- Generate default plots
- Generate convergence plots
- Store solution for all intermediate study steps

Information

Last computation time: 5 h 1 min 52 s



Messages Progress Log

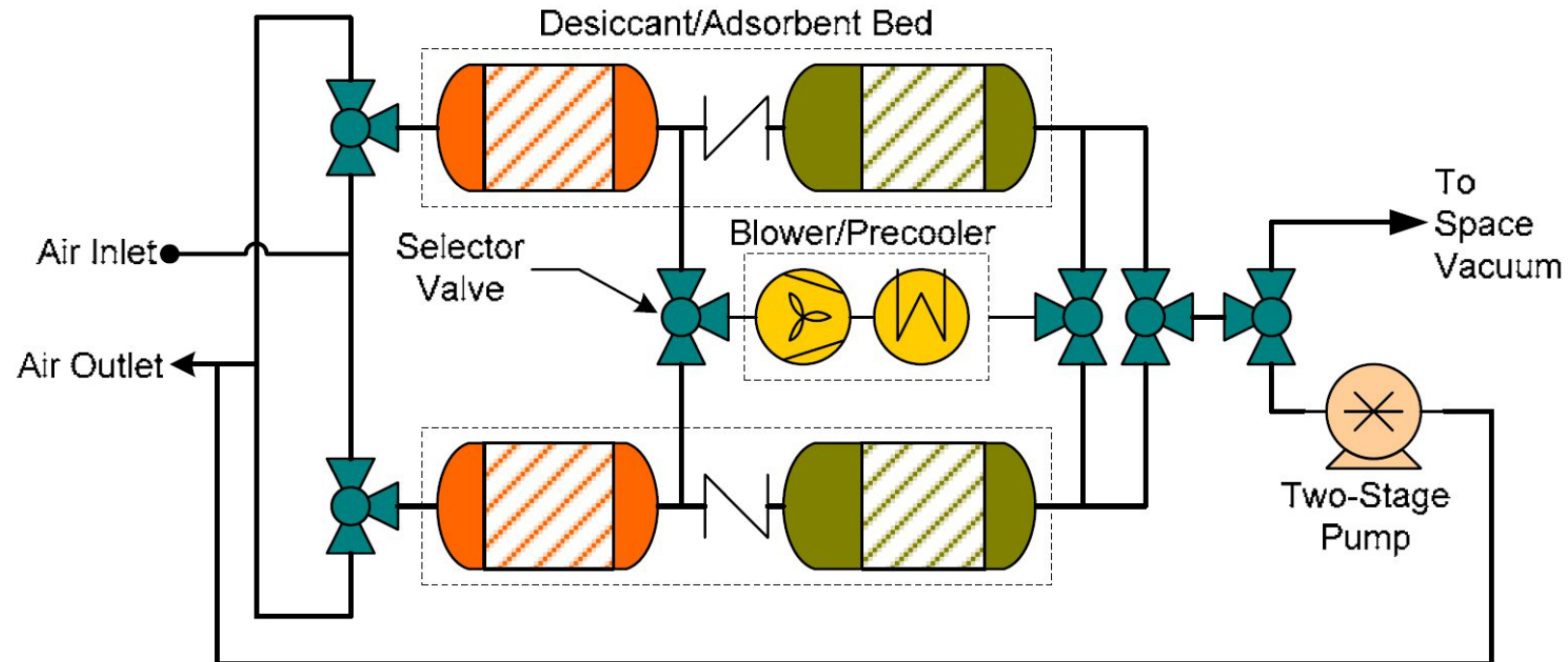
License will expire in 30 days.
 Opened file: asteroid_PDEs_17_v5.1.mph
 Complete mesh consists of 200 domain elements.
 Number of degrees of freedom solved for: 4005 (plus 10 internal DOFs).
 Number of degrees of freedom solved for: 10005 (plus 10 internal DOFs).
 Number of degrees of freedom solved for: 10005 (plus 10 internal DOFs).
 Number of degrees of freedom solved for: 10005 (plus 10 internal DOFs).
 Number of degrees of freedom solved for: 10005 (plus 10 internal DOFs).
 Opened file: CDRA-5_EC15_clean.mph
 Saved file: CDRA-5_EC15_clean.mph
 Saved file: CDRA-5_EC15_clean.mph
 Opened file: PDE_Adsorb.mph
 Saved file: PDE_Adsorb.mph
 Number of degrees of freedom solved for: 2965.
 Solution time (Study 1): 110 s. (1 minute, 50 seconds)
 Saved file: PDE_Adsorb.mph
 Number of degrees of freedom solved for: 2965.
 Solution time (Study 1): 112 s. (1 minute, 52 seconds)
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 Saved file: asteroid_PDEs_99_v5.1.mph
 Opened file: CDRA-5_EC15.mph

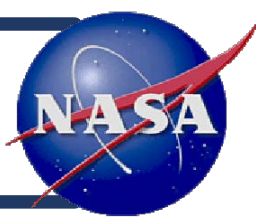


Introduction

- Advanced Exploration Systems (AES) Program:
 - pioneering approaches for rapidly developing prototype systems
 - validating concepts for human missions beyond Earth orbit
- Life Support Systems Project (LSSP):
 - mature environmental subsystems
 - **derived directly from the ISS subsystem architecture**
 - reduce developmental and mission risk
 - demonstrate concepts for human missions beyond Earth orbit

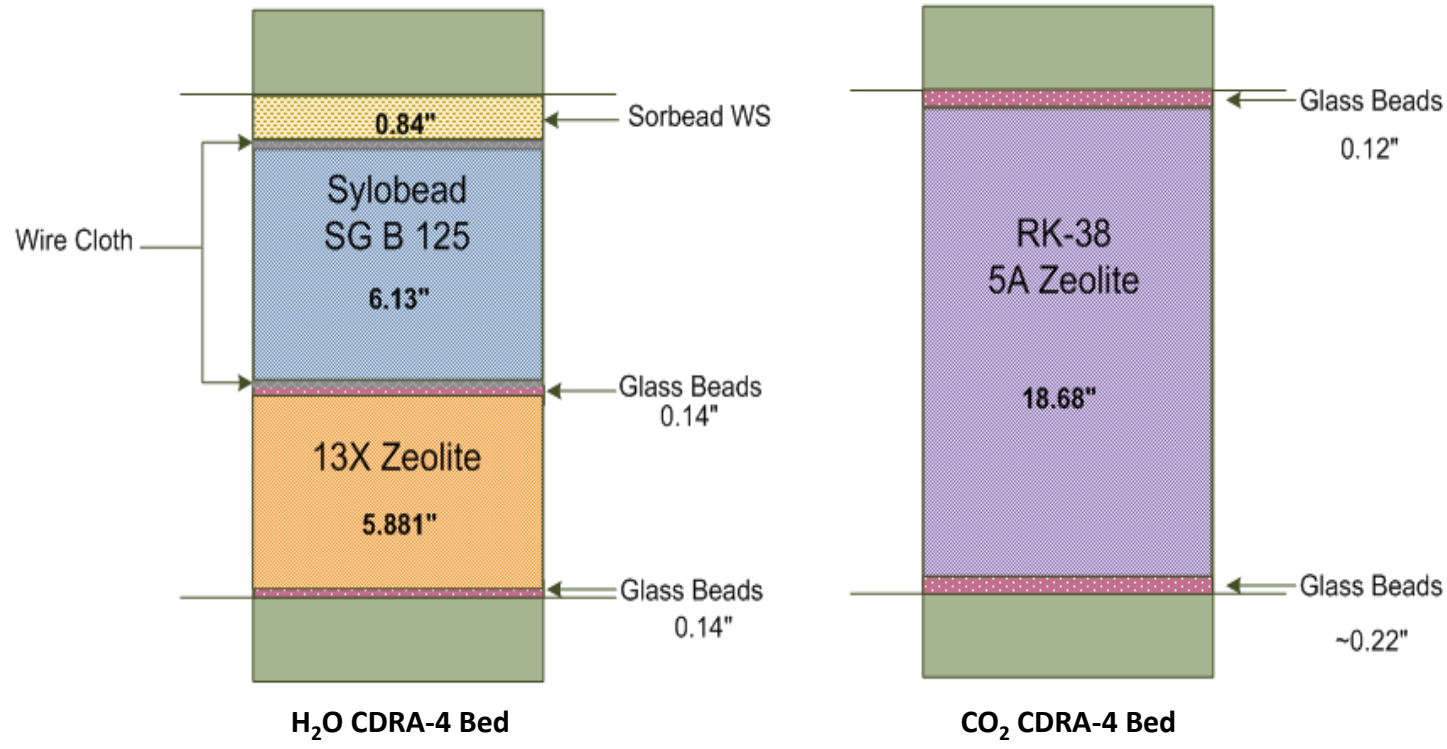
- Goal: *Predictive* model of the Carbon Dioxide Removal Assembly (CDRA)
- Here, focus on the 4 Bed Molecular Sieve (4BMS)
- Need to know sorbent behavior (isotherms, LDF, etc.)





The CDRA 4BMS Beds

- Multiple sorbents:
RK38 (5A), G544 (13X), Sorbead WS (SG), Sylobead B125 (SG)
- Multiple sorbates: CO₂, H₂O
- Variable flow rates, concentrations, and temperatures
- CO₂ bed desorbed with vacuum and in-situ heaters



- Insulated
- Square-ish cross sections
- Narrow RK-38 channels



Model Approach

- Use Toth isotherms from other work
- Use dimensionless correlations (Re, Nu, Pe, Pr, Sc)
 - Derives mass dispersion and thermal transfer coefficients
- Assume binary mass diffusion is valid
- Assume constant porosity
- Use Rumpf-Gupte permeability relationship
- Assume 1-D Darcy Flow
- Fit the single model parameter (LDF) using CBT data



COMSOL 4BMS Model

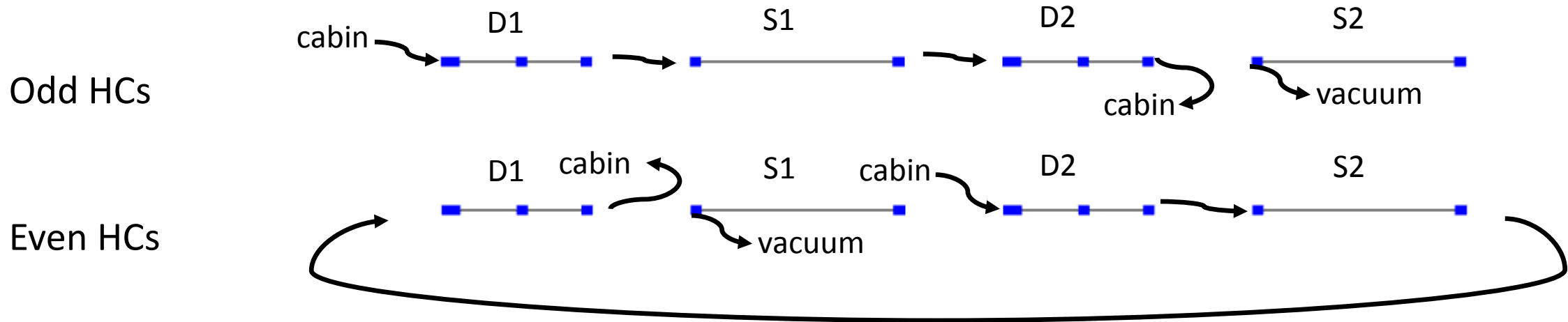


Use COMSOL Multiphysics to solve in 1-D:

- Transport of Concentrated Species (sorbate)
 - includes reactions, diffusion, and advection
 - time-dependent Mass Fraction inlet condition
- Heat Transfer
 - in solids for Can, Sorbent, and Insulation
 - Sorbent has sorption and heater Heat Sources
 - in fluids for Gas mixture
 - ideal gas with constant ratio of specific heats
 - time-dependent inlet Temperature condition
 - all are coupled via thermal coefficient Heat Sources
 - temperature-dependent material properties
- Darcy's Law (pressure and superficial velocity)
 - time-dependent inlet Mass Flux
 - estimated constant outlet Pressure
 - includes Mass Source due to sorption
- General Form PDE: pellet loading via LDF & Toth
- General Equations: heater switches



1-D Model



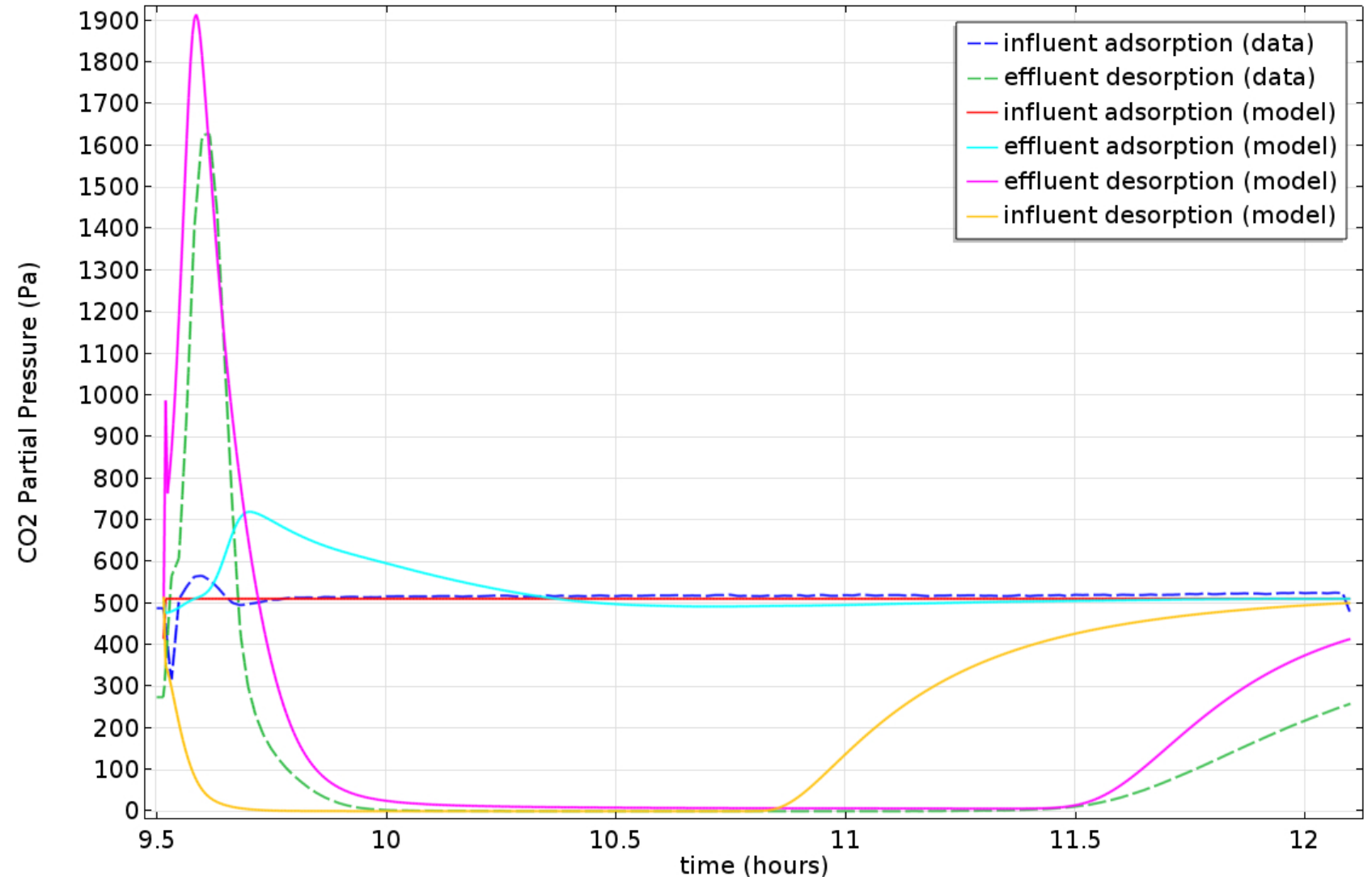
- Separate Physics Nodes and Steps for each bed
- Switch BC types for each half-cycle using Physics Tree
- Boundaries between sub-beds marked by ■



CDRA-4EU Test-bed CO₂ Results



- Competitive CO₂/H₂O on 13X (assumed 5 times 5A)
- 'burp' at start of HC reproduced
- Break-through at end of HC reproduced
- Requires heavy CO₂ loading of 13X and break-through of 5A
- 5A porosity of 55% (mass unknown)

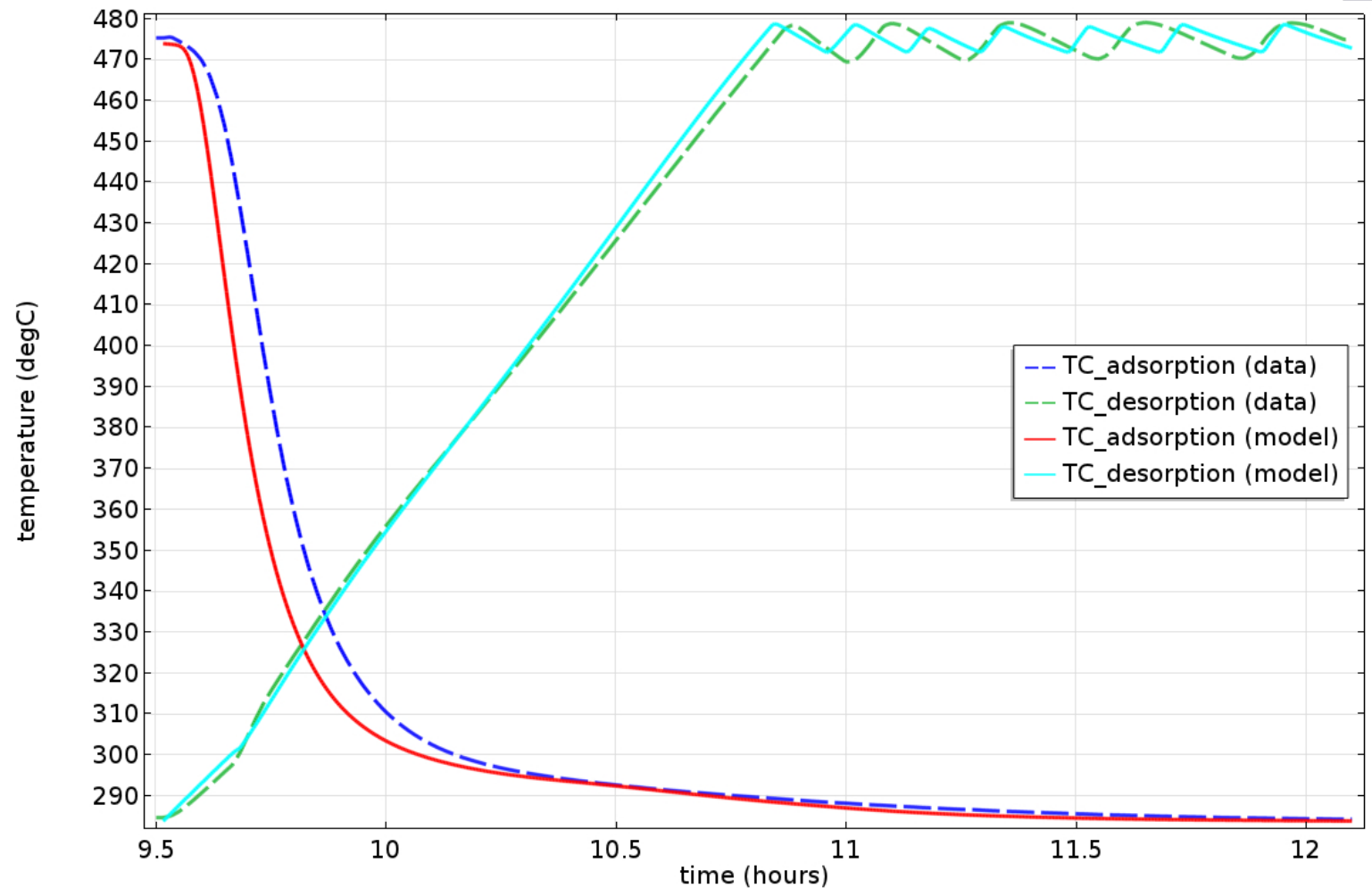




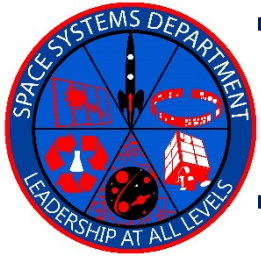
CDRA-4EU Test-bed Temperature Results



- Model cools too slightly too quickly during adsorption
- Heater control set-points in test appear 'soft'
- Slope, given thermal mass, dictates $\sim 670\text{W}$
- Model cools slightly too slowly during desorption when heaters off



Data only briefly heats at expected rate from 980W (but heater requirements say max 5 °F/min!)



Summary

- Have constructed a *predictive* CDRA 4BMS 1-D Comsol model
 - Calibrated with CBT on various sorbates, sorbents, flow rates, concentrations
- Generalize to 2D and 3D (?)
- Applied to CDRA-4EU Baseline data
 - Shows sorbent bed CO₂ breakthrough
 - Shows 13X CO₂ 'reservoir'
 - Do not remove 13X (without changing other things)!
 - Shows sorbent bed heater issue
- Approaching limits of 1-D
- Validate with more CDRA4-EU tests
 - Different flow-rates, half-cycle times, dew points, vapor pressures
- Inform CDRA optimization
- Genuine H₂O/CO₂ sorption competition model

→ Virtual Laboratory of the CDRA System