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Numerical Simulation of Electrolyte-Supported Planar Button Solid Oxide Fuel Cell

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Objectives

- Build a working model of planar buttonshaped electrolyte supported SOFC
- Run simulations for several electrolyte material configurations
- Study effect of electrolyte on performance

Solid Oxide Fuel Cell (SOFC)

SOFC

- ✓ Solid electrolyte Ceramics
- ✓ Operating temperatures (400°C 1000°C)



Advantages of SOFC

- ✓ High efficiency (>50%, >80% CHP) [1]
- ✓ Fuel flexibility (H_2 , natural gas, biogases, etc.)
- ✓ Combined Heat & Power generation
- ✓ Compatible with gas & steam turbines
- ✓ Power output (W to MW)
- ✓ Relatively higher power density
- \checkmark No water flooding issues, unlike PEMFC

 $H_2 \rightarrow 2H^+ + 2e^-$

 $\frac{1}{2}O_2 + 2H^+ + 2e^- \rightarrow H_2O$

Picture Source: U.S. Department of Energy website

Types of Planar SOFC



Source: Mark C. Williams, Joseph P. Strakey and Wayne A. Surdoval, U.S. Department of Energy's Solid Oxide Fuel Cells: Technical Advances, Int. J. Appl. Ceram. Technol., 2 (4) 295–300 (2005)

Electrolyte Materials – YSZ, SCSZ

Ideal electrolyte – high ionic conductivity, phase stability, mechanical strength.

SCSZ - $Sc_{0.17}Ce_{0.08}ZrO_2$ YSZ - 8 mol% Y_2O_3 stabilized ZrO_2

• SCSZ electrolyte will be ideal in terms of conductivity.

• SCSZ undergoes phase transition (cubic to rhombohedral) at 300-500 °C.

• YSZ is stable in both oxidizing and reducing environments, maintains cubic structure.

Electrolyte Supported Design





SOFC Material Properties

	Anode – Ni- YSZ	Cathode - LSCF	Electrolyte – YSZ	Electrolyte - SCSZ
Ionic Conductivity [S/m]	1	5.15	4.24 – 4.62	10.58 – 11.93
Electronic Conductivity [S/m]	650000	2300	negligible	negligible
Porosity	40 %	40 %	0	0
Cathode \longrightarrow Electrolyte \longrightarrow			<pre>- LSCF* - YSZ - SCSZ</pre>	
Anode —→	× 400 15	10µm JEOL 7/16 .0kV SEI LM WD 11.0mm 3	→ YSZ → Ni-YSZ	

LSCF* - $(La_{0.6}Sr_{0.4})_{0.95-0.99}Co_{0.2}Fe_{0.8}O_3$

SOFC Geometry: Top View



SOFC Geometry



Anode & Cathode thickness	50 µm
Electrolyte layer thickness	30 µm
Anode & Cathode diameter	10 mm
Electrolyte diameter	20 mm
Gas flow channel height (Anode & Cathode)	1 mm
Gas flow channel diameter (Anode & Cathode)	10 mm

Modeling Methodology

COMSOL:

Electrochemistry – Current distribution & Transport of chemical species

Current distribution	Transport of chemical species
$\nabla \cdot j = Q$	Maxwell-Stefan diffusion model:
$j = \sigma \nabla \Phi$	$\frac{\partial}{\partial t}(\rho\omega_i) + \nabla \cdot (\rho\omega_i u) = \nabla \cdot m_i + R_i$
$\eta_m = \Phi_s - \Phi_l - E_{eq,m}$	$\sum_{r=1}^{Q} \sum_{r=1}^{Q} \sum_{r=1}^{T} \nabla T$
Butler-Volmer equation:	$m_i = \rho \omega_i \sum_{k=1}^{n} D_{ik} d_k + D_i^{T} \frac{1}{T}$
$j = j_o \left[\left(\frac{c}{c_0} \right)_R exp \left\{ \frac{n\alpha F}{RT} \eta \right\} - \left(\frac{c}{c_0} \right)_P exp \left\{ \frac{-n(1-\alpha)F}{RT} \eta \right\} \right]$	<i>k</i> =1
j = i/area [A/m²], current density vector	ρ: mixture density (kg/m³)
Q – source or sink term	u: mass average velocity (m/s)
$\Phi_{\rm I}, \Phi_{\rm s}$ - electrolyte and electrode potential respectfully [V]	ω_i : mass fraction
σ - electrolyte conductivity [S/m]	j _i : mass flux relative to the mass average velocity
η – activation overpotential [V]	$(kg/(m^2s))$
E _{eq,m} - equilibrium potential for the m reaction	R _i : consumption or production rate (kg/(m ³ s))
i_{R} – reference current density	D^{T} : thermal diffusion coefficients (kg/(ms))
n: number of charges transferred	D_i : diffusional driving force acting on species k (1/m)
α : transfer coefficient	\widetilde{D}_{ik} : multicomponent Fick diffusivities (m ² /s)

Modeling Methodology

Fluid mechanics – Brinkman equations (porous media)

Continuity equation:

$$\frac{\partial}{\partial t}(\varepsilon_p \rho) + \nabla \cdot (\rho u) = Q_{br}$$

For incompressible fluids:

 $\rho \nabla \cdot u = Q_{br}$

Momentum equation:

$$\frac{\rho}{\varepsilon_p} \left(\frac{\partial u}{\partial t} + (u \cdot \nabla) \frac{u}{\varepsilon_p} \right) = -\nabla p + \nabla \cdot \left[\frac{1}{\varepsilon_p} \left\{ \mu (\nabla u + (\nabla u)^T) - \frac{2}{3} \mu (\nabla \cdot u) I \right\} \right] - \left(\frac{\mu}{k} + Q_{br} \right) u + F$$

 μ : dynamic viscosity of the fluid (Pa·s)

- u : velocity vector (m/s)
- ρ : fluid density (kg/m³)
- p : pressure (Pa)
- ϵ_p : porosity
- k : permeability of porous medium (m²)
- Q_{br} : mass source or mass sink (m³/s)
- F : volume forces vector (kg/m²s²)

Results



6 - Layered Electrolyte



• Pure SCSZ electrolytes had highest power

Lower ohmic losses

Comparison of YSZ, YSZ-SCSZ Layered, and SCSZ Single Cell Performance



Conclusion & Future Work

- Using SCSZ as the electrolyte material yields the best performance, i.e., the maximum power and current density.
- As the number of electrolyte layers increases, the performance decreases (higher ohmic losses).
- Future work will include incorporating heat transfer physics.
- Compare and match the i-V plot and other experimental results when the SOFCs are produced and tested in the lab.
- Use model to calculate parameters (α, j_o) by curve fitting with experimental results.
- Finite Element Modeling of SOFC electrolyte to find relationship between load, fracture strength and deflection.

Questions? Thank you!

References

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