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15 – OCTOBER – 2015

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**COMSOL
CONFERENCE**
2015 GRENOBLE

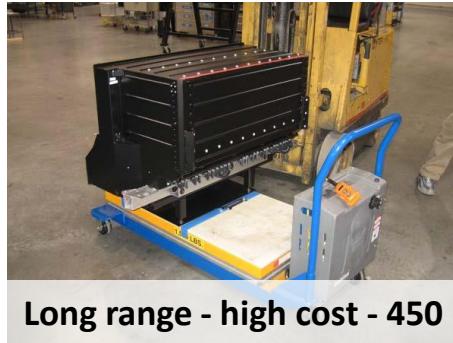


BATTERY PACK APPROACHES

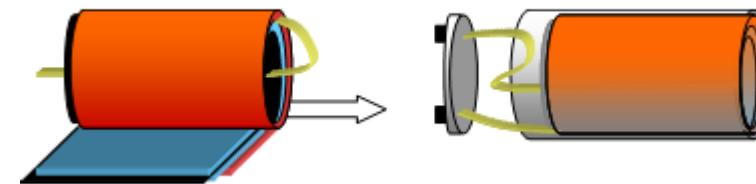
THE BATTERY PACK ASSIGNS THE ELECTRICAL VEHICLE'S PERFORMANCES



Sport car



Long range - high cost - 450 kg



2.4 Ah / 45g – 190 Wh/kg



Family car



Mid range - moderate cost - 230 kg



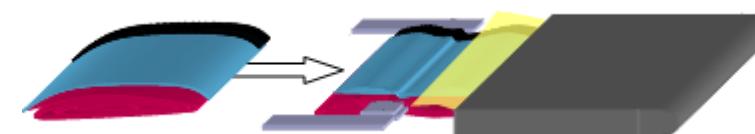
32 Ah / 1kg – 130 Wh/kg



Urban car

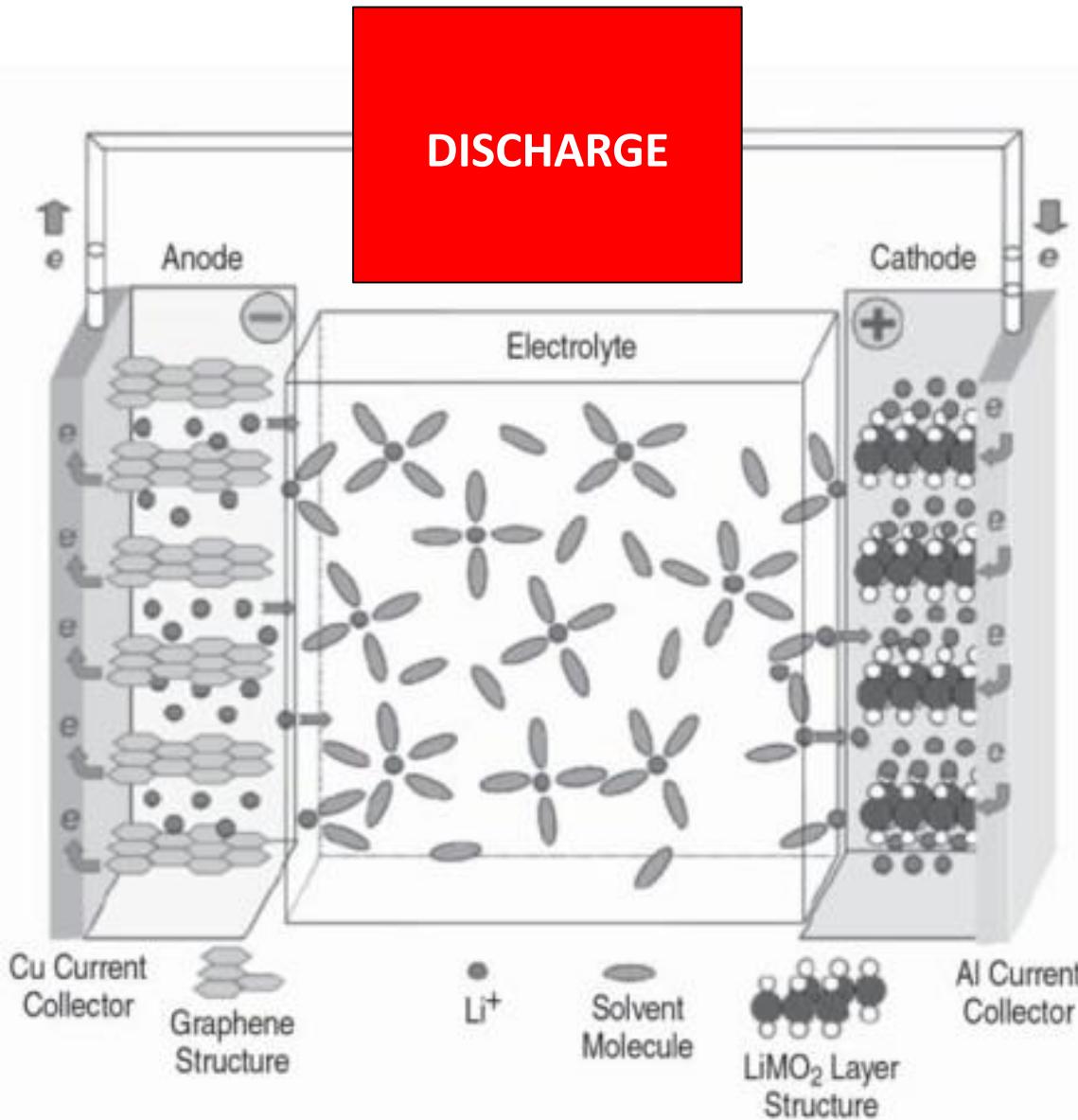


Low range - low cost - 200 kg



50 Ah / 1.7 kg – 110 Wh/kg

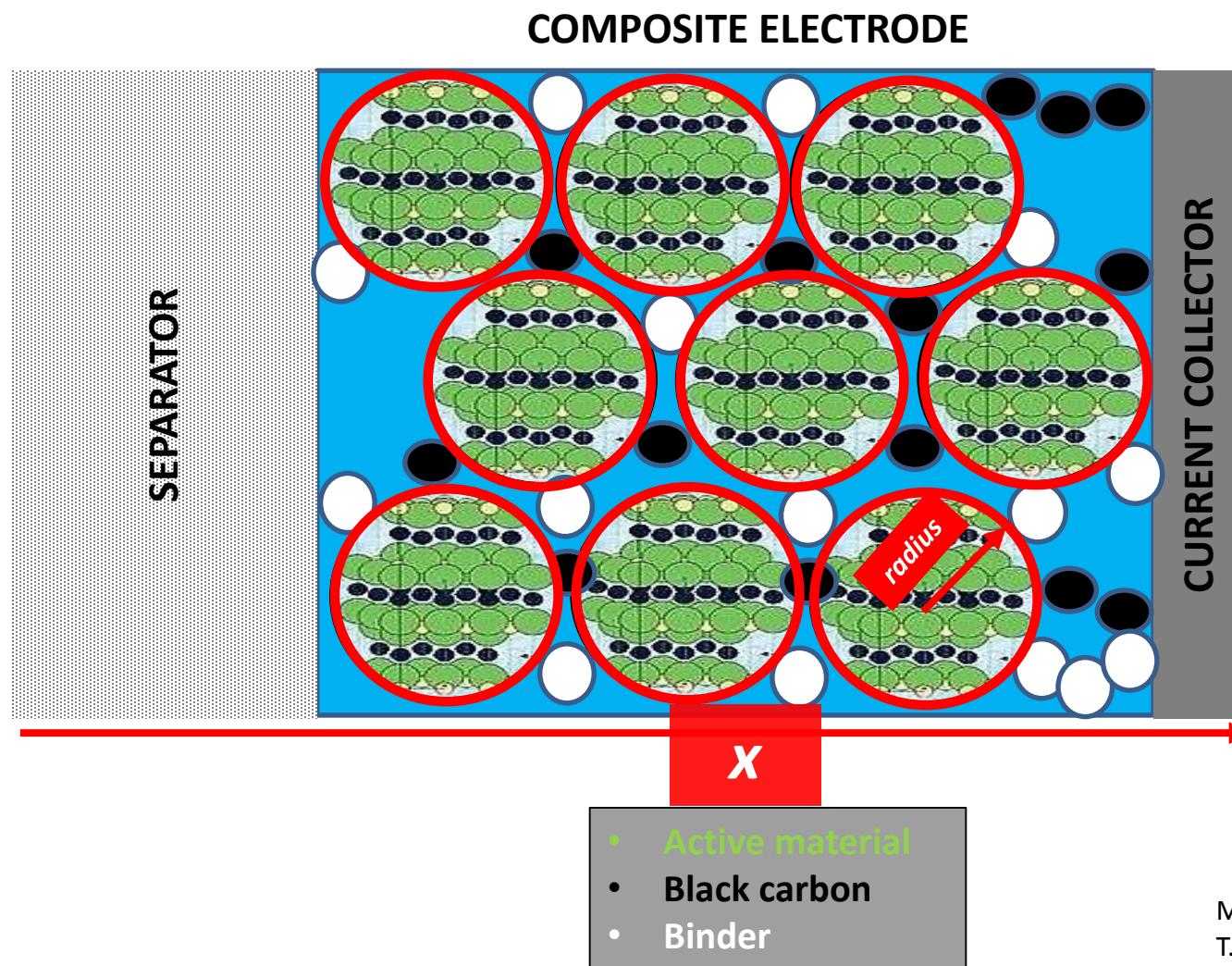
HOW DO LITHIUM-ION BATTERIES WORK?



INTERCALATION REACTION

- Negative : $C + xLi^+ + xe^- \xrightleftharpoons[\text{charge}]{\text{discharge}} Li_xC$
- Positive : $LiMO_2 \xrightleftharpoons[\text{charge}]{\text{discharge}} Li_{1-x}MO_2 + xLi^+ + xe^-$

POROUS THEORY BASED MODEL



- 12 EQUATIONS SOLVED WITH COMSOL
- 27 VOLUME AVERAGED PARAMETERS

- *Liquid phase ideal mass transport (migration + diffusion)*
- *Liquid phase potential (ionic Ohm law)*

- *Solid phase diffusion*
- *Solid phase potential (electronic Ohm law)*

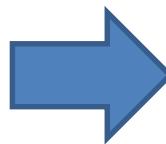
- *Li⁺/Li charge transfer (Insertion reaction kinetics)*

M. Doyle, et. al., J. Electrochem. Soc. 140 (1993) 1526
T. F. Fuller, M. Doyle and J. Newman, J. Electrochem. Soc., 141 (1994)

NON DIMENSIONAL EQUATIONS

Adimensionnalization

- Parameters from 27 to 16
- Generalize the simulation results
- Highlight some parameters connections
- Identification of the system time constants



Dimensionless	
$\tilde{t} = t \frac{1}{\varepsilon_{+l}} \frac{D_{e+}}{d_+^2}$	Time
$\tilde{j} = j \frac{d_+}{D_{e+} F C^*}$	Current
$\tilde{\varphi} = \frac{F}{RT} \varphi$	Voltage
$\tilde{x} = \frac{x}{d_{+-e}}$	Thickness

- $\tilde{t} = \frac{t}{89 [s]}$
- $\tilde{j} = \frac{j}{14.3 [Am^{-2}]}$
- $\tilde{\varphi} = \frac{\varphi}{25 [mV]}$
- $\tilde{x} = \frac{x}{60 [\mu m]}$

CLASSIC DISCHARGE @ 1C-rate*:
 $\tilde{j} \cong 2$
 $\tilde{t}_{100 \% \text{ soc}} \cong 40$



Derived

$A_{1\pm} = \frac{RT}{F} \frac{\sigma_\pm}{D_{e\pm} F C^*}$	Electronic conduction vs Li diffusion in the electrolyte
$A_{2\pm} = \varepsilon_{\pm s} \frac{D_{s\pm}}{D_{e\pm}} \frac{C_{s,max\pm}}{C^*} \left(\frac{d_\pm}{R_{p\pm}} \right)^2$	Solid phase diffusion vs Li diffusion in the electrolyte

*VALUES FROM LITERATURE:

L. Zhang et al., Energies 2014, 7, 6282-6305

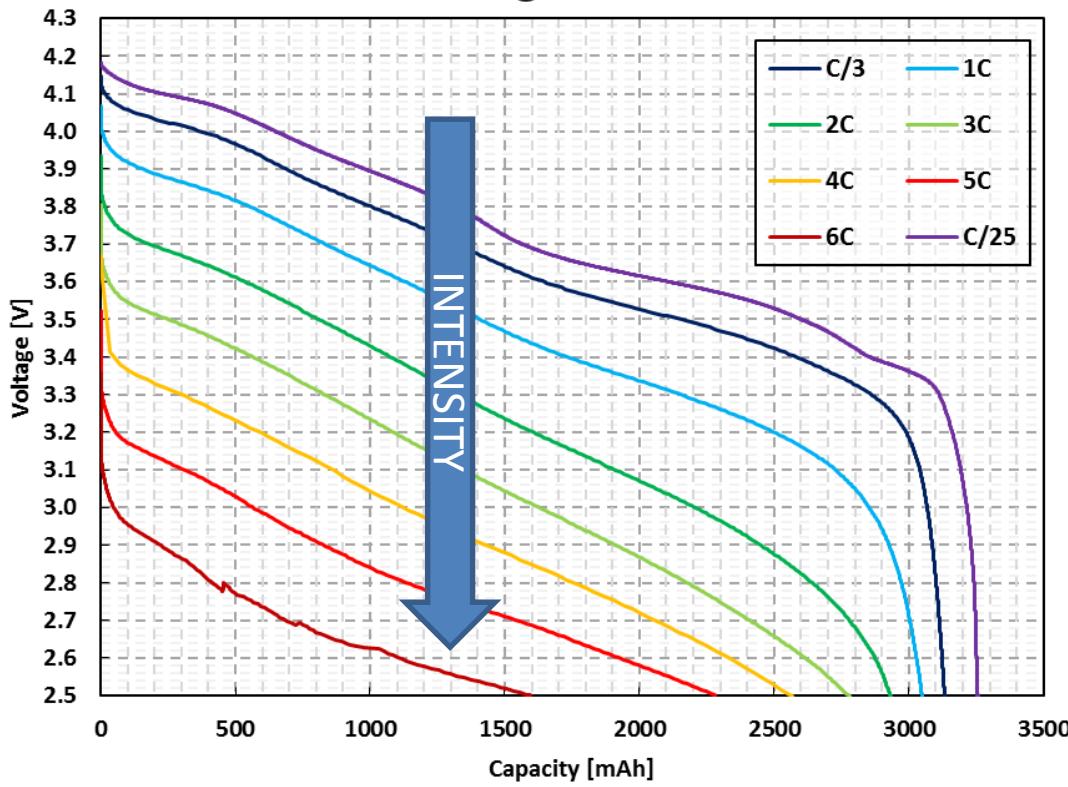
L. Valøena et al., J. Electrochem. Soc. 152 (5) A882-A891 (2005)

EXPERIMENTAL RESULTS ON HIGH ENERGY DENSITY CELL

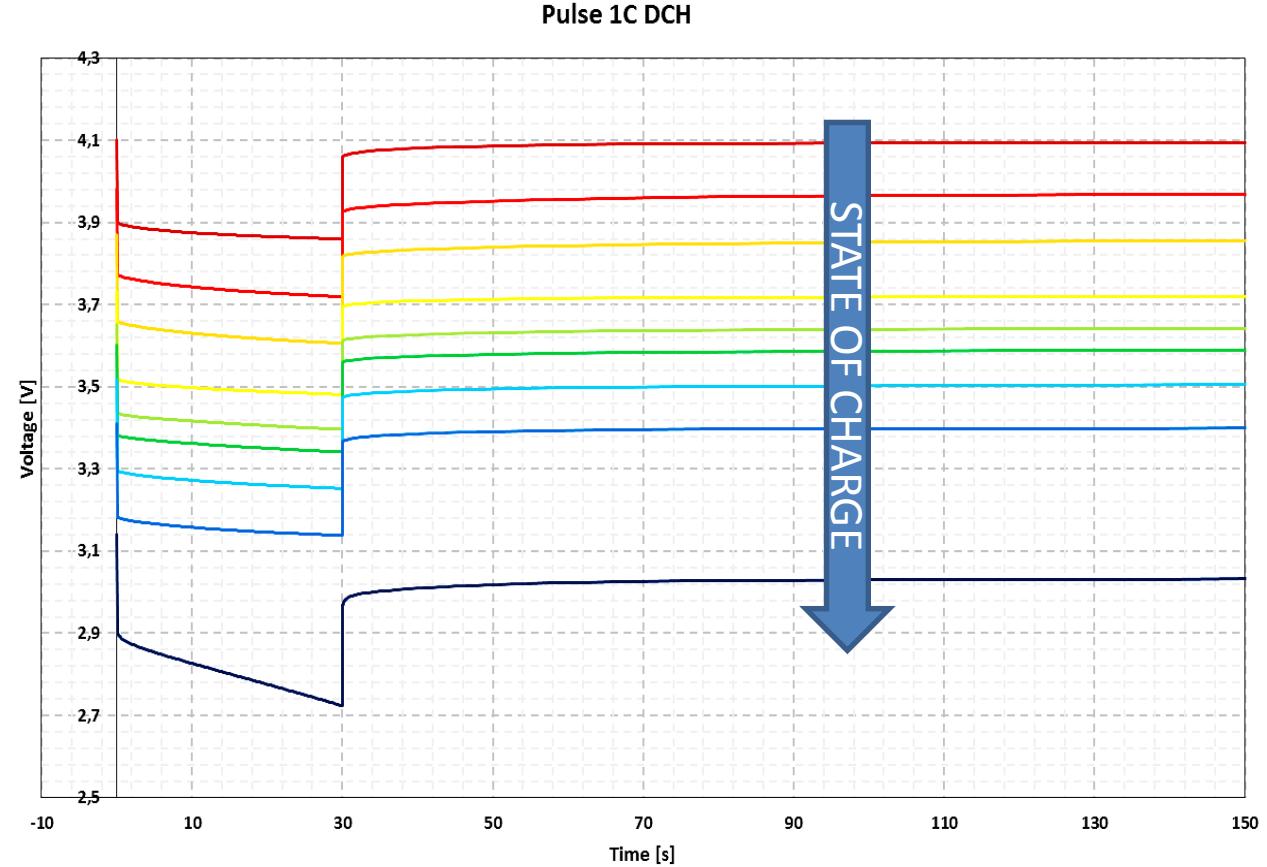
COMMERCIAL CELL CHARACTERIZATION

- PREDICT THE PRACTICAL CAPACITY ;
- IDENTIFY IMPULSIONS AND RELAXATION PHENOMENA

Discharge @ 25°C



Pulse 1C DCH

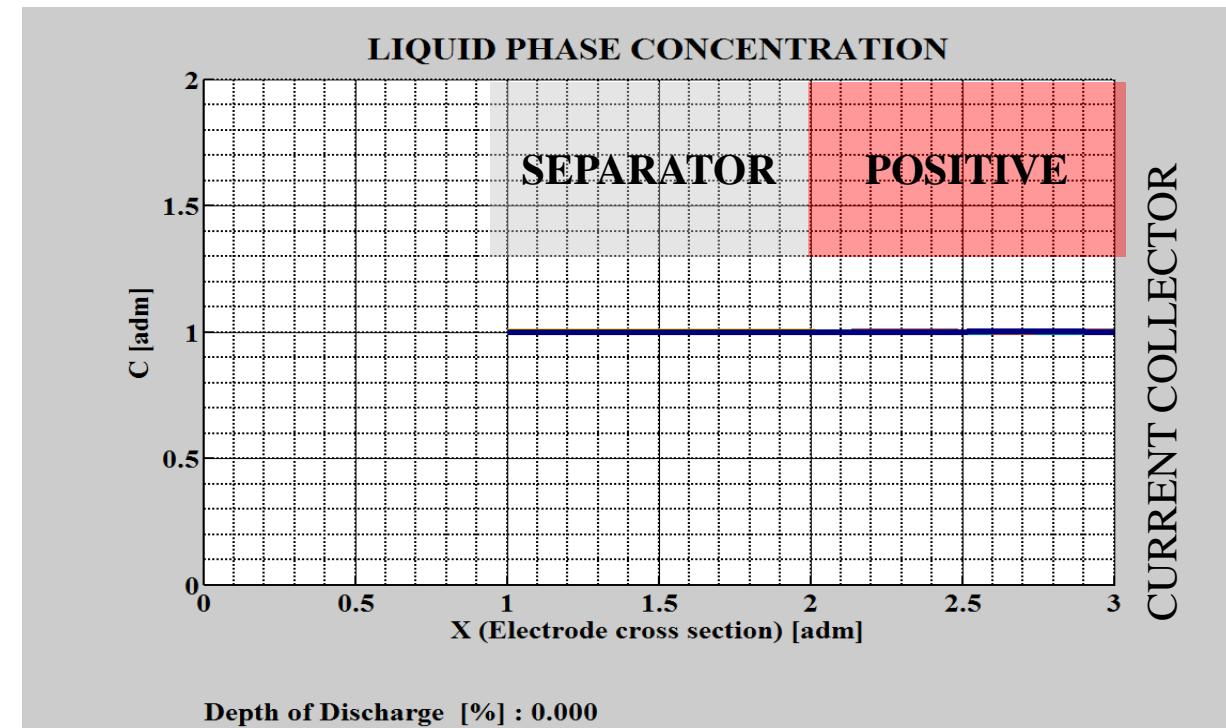
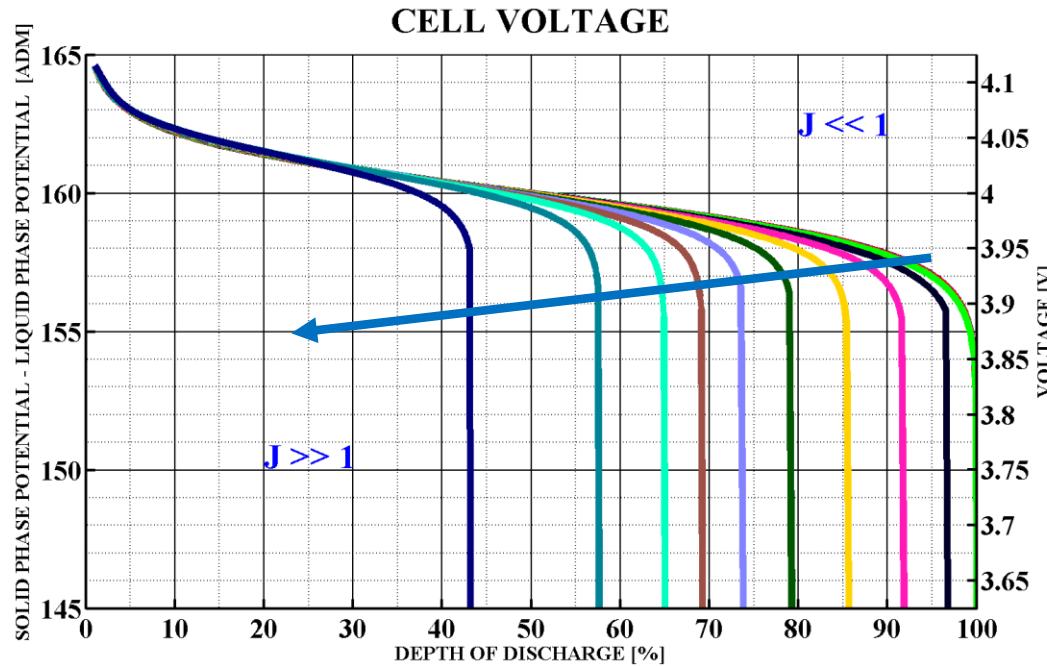


- SMOOTH END OF DISCHARGE DUE TO CUT OFF VOLTAGE.

GALVANOSTATIC DISCHARGE SIMULATION : VARIABLE CURRENT DENSITY

CONFIGURATION

- $A_{1\pm} = \frac{RT}{F} \frac{\sigma_\pm}{D_{e\pm} F C^*}$ (High Electronic Conductivity)
- $A_{2\pm} = \varepsilon_{\pm s} \frac{D_{s\pm}}{D_{e\pm}} \frac{c_{s,max\pm}}{C^*} \left(\frac{d_\pm}{R_{p\pm}} \right)^2$ (High Solid Diffusivity)



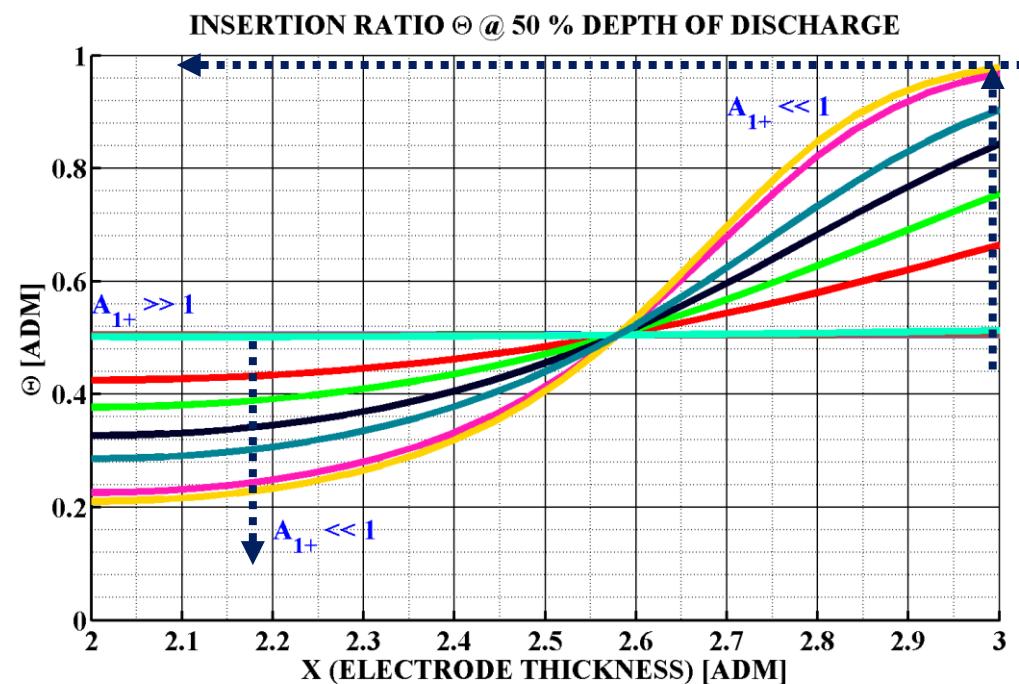
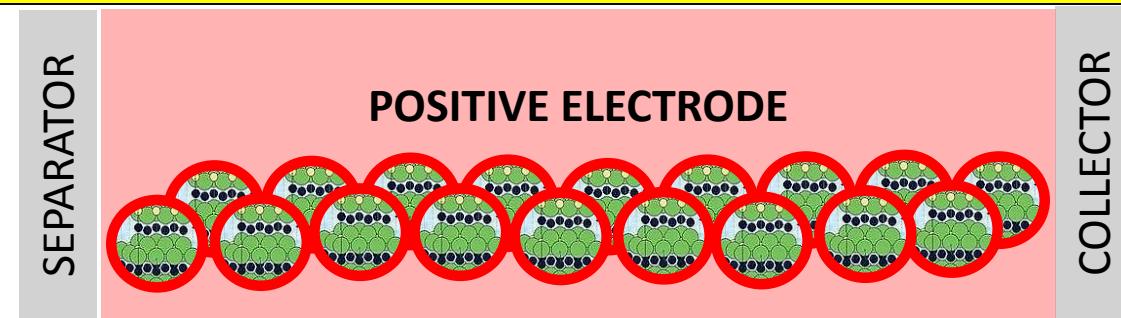
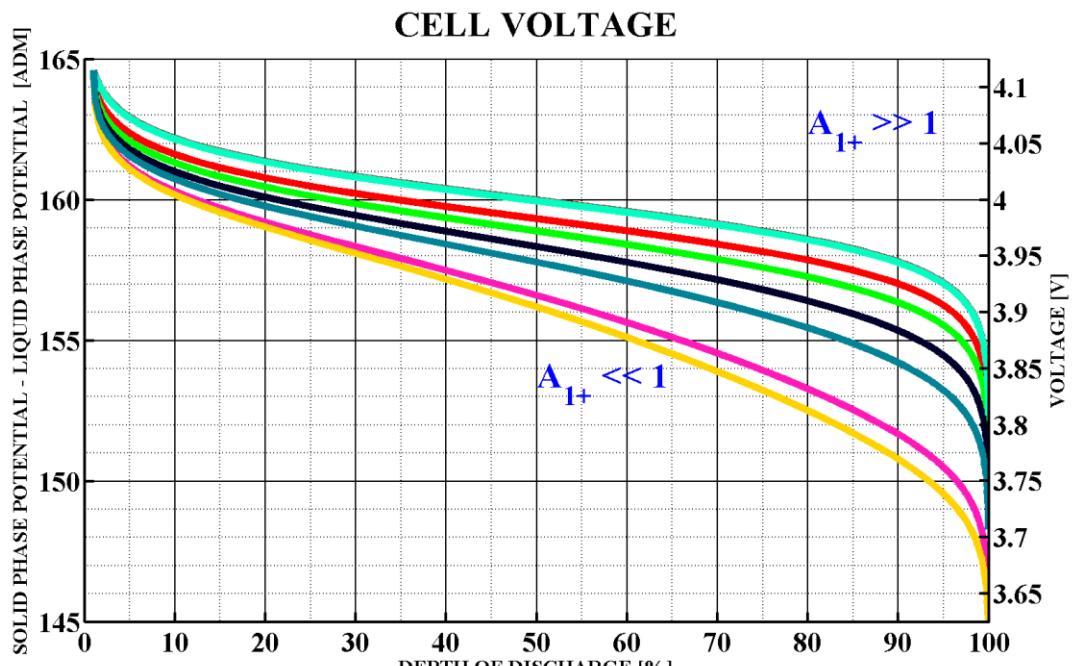
- DISCHARGE LIMITATION DUE TO Li⁺ DEPLETION

GALVANOSTATIC DISCHARGE SIMULATION : VARIABLE CONDUCTIVITY

CONFIGURATION :

- High Solid Diffusivity
- Variable electronic conductivity ;
- $J \ll 1$ (Constant Li⁺ concentration in the electrolyte)

$$A_{1\pm} = \frac{RT}{F} \frac{\sigma_{\pm}}{D_{e\pm} F C^*}$$



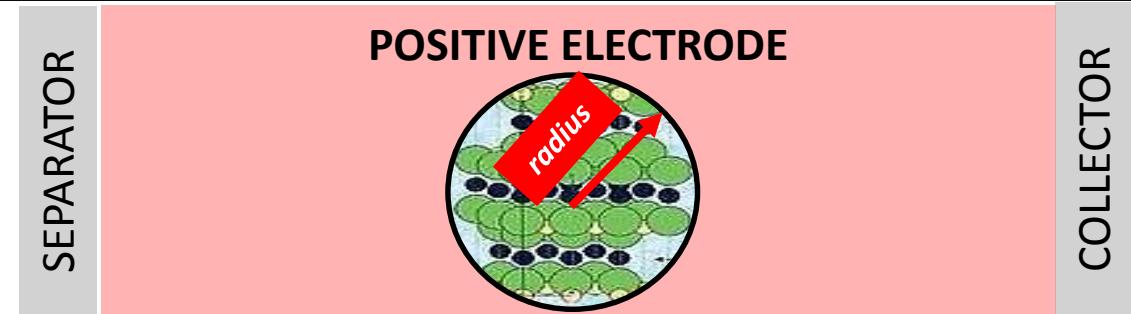
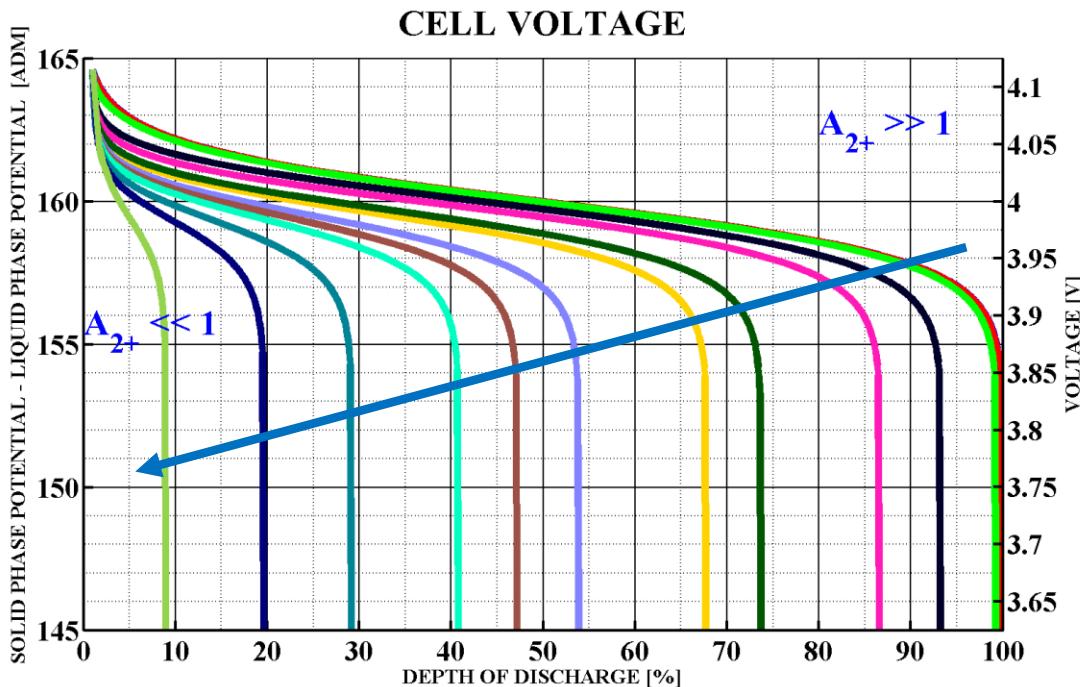
- POLARIZATION DUE TO SOLID PHASE CONCENTRATION
- THE INSERTION RATIO @ 50 % IS HIGHER AT COLLECTOR AND LOWER NEAR THE SEPARATOR BECAUSE THE ELECTRONS MINIMIZE THE PATH;

GALVANOSTATIC DISCHARGE SIMULATION : VARIABLE DIFFUSIVITY

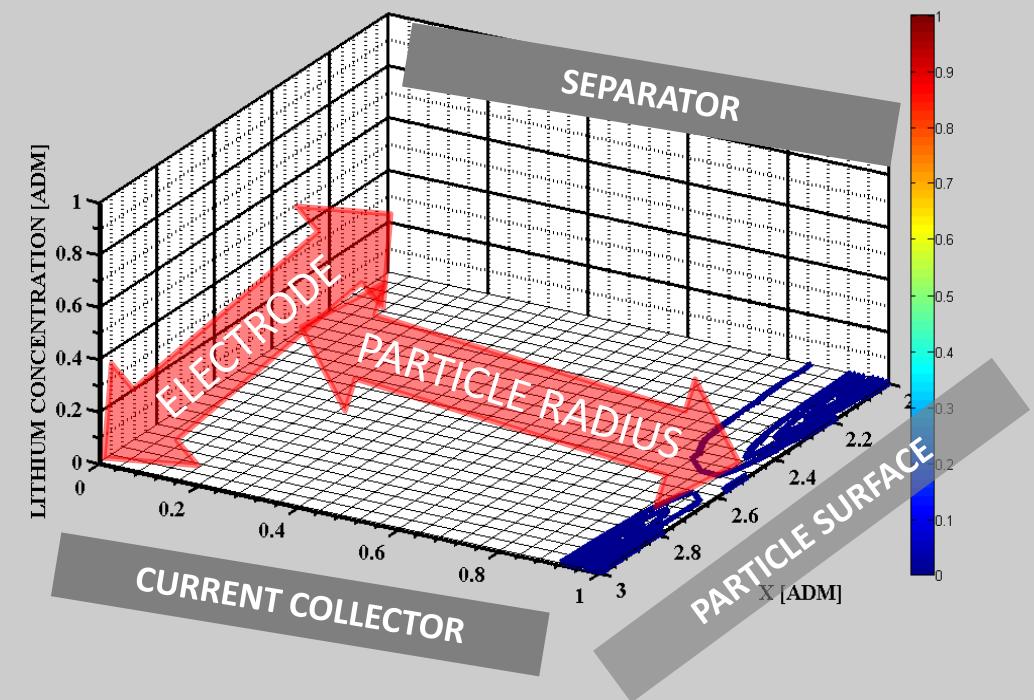
CONFIGURATION :

- High Conductivity
- Variable solid phase diffusivity
- $J \ll 1$ (Constant Li⁺ concentration in the electrolyte)

$$A_{2\pm} = \epsilon_{\pm s} \frac{D_{s\pm}}{D_{e\pm}} \frac{C_{s,max\pm}}{C^*} \left(\frac{d_\pm}{R_{p\pm}} \right)^2$$



POSITIVE ELECTRODE SOLID PHASE CONCENTRATION

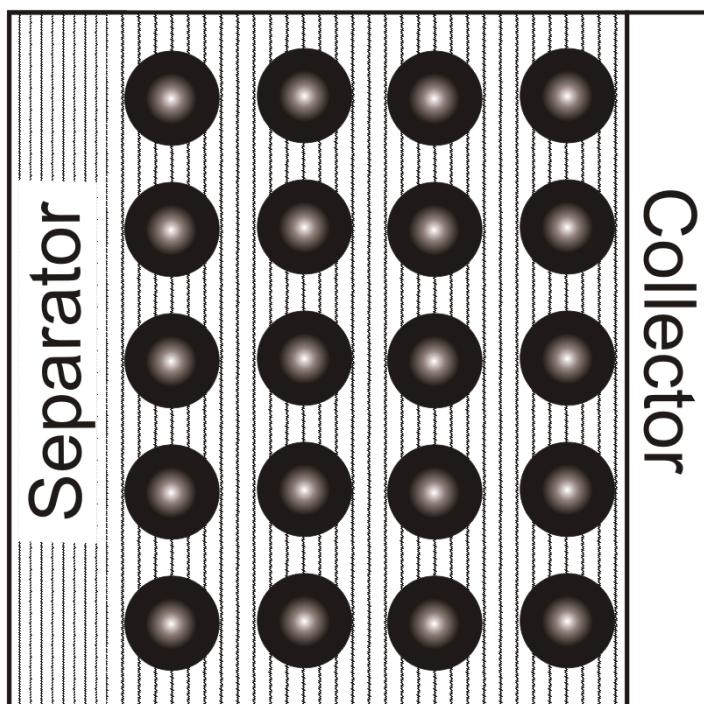


- WHEN THE EXTERNAL CONCENTRATION REACHES 1 FOR ALL THE PARTICLES THE DISCHARGE IS OVER;

DISCHARGE INTERRUPTION PHENOMENA RESUMED

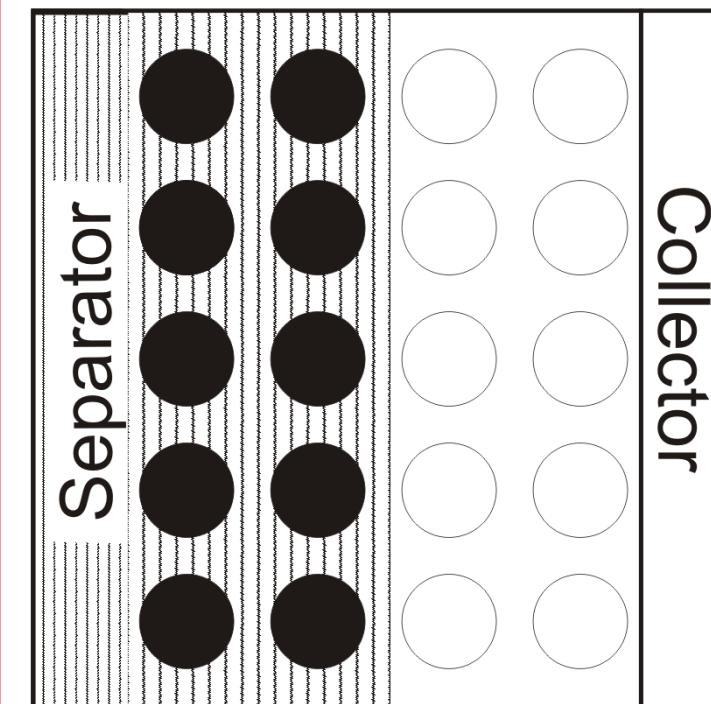
Solid Phase Diffusion

Lithium accumulation at particles surface



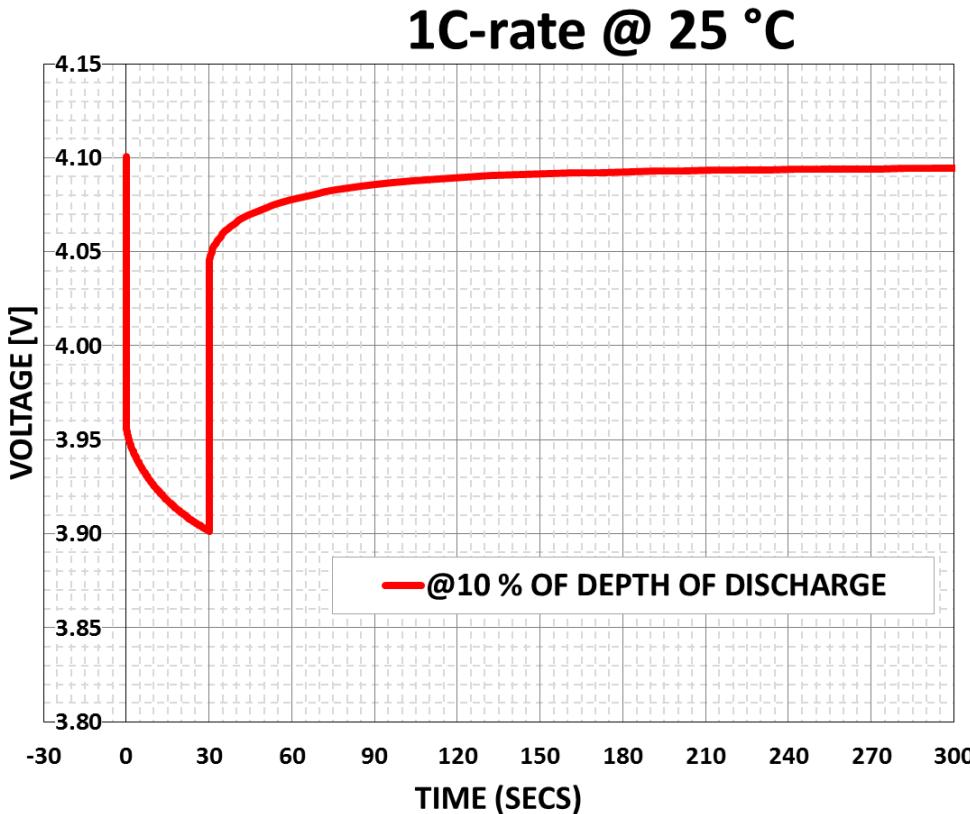
Liquid Phase Diffusion

Lithium depletion in the electrolyte



DIRECT CURRENT RESISTANCE

EXPERIMENTAL

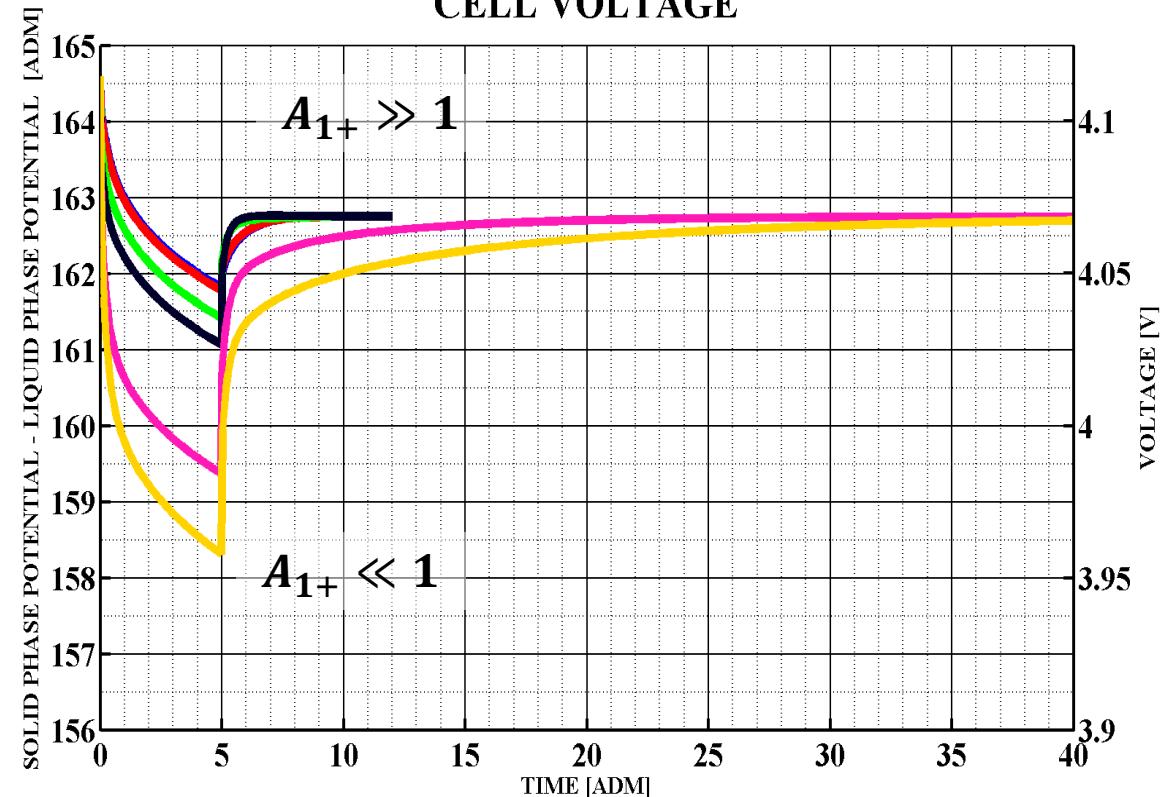


SIMULATION

- Variable electronic conductivity
- $J = 1$

$$A_{1\pm} = \frac{RT}{F} \frac{\sigma_{\pm}}{D_{e\pm} F C^*}$$

CELL VOLTAGE



- THE VOLTAGE PROFILE IS REPRODUCED WITH THE RELAXATION
- THE SOME PARAMETERS COULD BE IDENTIFIED WITH PULSES AND RELAXATIONS

CONCLUSIONS

- Dimensionless simulation of Lithium ion cell discharge with COMSOL coefficient form pde.
- Identify different limiting discharge phenomena and reduction of parameters.

SHORT TERM PERSPECTIVES

- Find other limiting factors and conditions.
- Create specific tests for the parameters tuning.

THANK YOU FOR YOUR ATTENTION. QUESTIONS ?